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140 MAYFAIR ROAD, SUITE 900 HATTIESBURG, MS 39402



PHONE: 601-428-7725 Fax: 601-450-4448

February 24, 2025

Mr. Jeffrey Bland, P.E. **Environmental Permits Division** Mississippi Department of Environmental Quality PO Box 2261 Jackson, MS 39225-2261

Dear Mr. Bland:

Re:

Venture Oil & Gas Inc. Stone 9-5 No. 1 Tank Battery, AI 82364

MSOPGP1300-00086

Oil Production General Permit NOI Modification

Venture Oil & Gas Inc. is submitting the enclosed NOI for modification of coverage under the Oil Production General Permit for the Stone 9-5 No. 1 facility in Jasper County, MS. The compressor engine identified as 150 hp in the original submittal will instead utilize a 215 hp engine. Enclosed are the updated application forms and emissions calculations. If you have any questions, please feel free to contact me at (601) 428-2257.

Sincerely,

Dan Watts **EHS Director**

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Facility (Agency Interest) Information	Section OPGP - A
1. Name, Address, and Location of Facility	10 mm from 5
A. Owner/Company Name: Venture Oi	l & Gas Inc.
B. Facility Name (if different than A. above):	Venture Stone 9-5 No. 1 Facility
C. Facility Air Permit/Coverage No. (if known)	MSOPGP1300-00086
D. Agency Interest No. (if known):	82364
E. Physical Address 1. Street Address: Field Road off of Jasp 2. City: Stringer	er County Road 713 3. State: MS
4. County: Jasper	5. Zip Code: <u>39481</u>
6. Telephone No.: 601-518-0622	7. Fax No.:
8. Are facility records kept at this location?	Yes No. Please complete Item 10.
2. City: Laurel 4. Zip Code: 39440 G. Latitude/Longitude Data 1. Collection Point (check one): ☐ Site Entrance 2. Method of Collection (check one): ☐ GPS Specify coordinate sys ☐ Map Interpolation (Google Earth, of the system) 3. Latitude (degrees/minutes/seconds): 4. Longitude (degrees/minutes/seconds): 5. Elevation (feet): 350 H. SIC Code: 1311	i i i i i i i i i i i i i i i i i i i
2. Name and Address of Facility Contact	
A. Name: Dan Watts	Title: EHS Director
and sales as a second sales and	ir Road, Suite 900
2. City: Hattiesburg	3. State: MS
4. Zip Code: 39402	5. Fax No.: <u>601-450-4448</u>
6. Telephone No.: 601-428-2257	
7. Email: dwatts@venture-inc.com	•

Facility (Agency Interest) Information	Section OPGP - A
3. Name and Address of Air Contact (if differe	ent from Facility Contact)
A. Name:	Title:
B. Mailing Address	
1. Street Address or P.O. Box:	
2. City:	3. State:
4. Zip Code:	5. Fax No.:
6. Telephone No.:	
7. Email:	
A Name and Address of Description Officials	C Al To 114.
4. Name and Address of Responsible Official factorial The Form must be signed by a Responsible Official as	
The Form must be signed by a Responsible Official as	defined in 11 Miss. Admin. Code 1 i.2, R. 2.1.C(24).
A. Name: Adam Barham	Title: VP-operations
A. Name. Adam Barian	Title. VI-operations
B. Mailing Address	
<u> </u>	Road, Suite 900
2. City: Hattiesburg	3. State: MS
4. Zip Code: 39402	5. Fax No.: 601-450-4448
6. Telephone No.: 601-518-0624	
7. Email: abarham@venture-inc.com	
C. Is the person above a duly authorized represen	ntative and not a corporate officer?
.□ Yes ☑ No	
If yes, has written notification of such authorizati	ion been submitted to MDEO?
Yes No	Request for authorization is attached
5. Type of Oil Production Notice of Intent (Ch	eck all that apply)
☐ Initial Coverage	☐ Re-Coverage for existing Coverage
☐ Modification with Public Notice	☑ Modification without Public Notice
iviodification with I dolle Notice	— Modification without I ubite Notice
☑ Update Compliance Plan	
• •	

EMISSIONS EQ	QUIPMENT AT A SYNTHETIC M	INOR SOURCE
Facility (Agency Interest) Information	Section OPGP - A
6. Equipment List (Chec.	k all that apply)	
Complete supporting emission	n calculations must be included for each potential	emission unit selected below.
 ✓ Heater Treater. Include a ✓ Condensation Storage V ✓ Water Storage Vessel. In ✓ Internal Combustion Eng ✓ Flare. Include a complet ✓ Oil Truck Loading (Sect 	a completed Section OPGP-C Form for each unit essel. Include a completed Section OPGP-E Form actude a completed Section OPGP-E Form for ea gine. Include a completed Section OPGP-D Form ed Section OPGP-F Form for each unit.	t. <u>m</u> for each unit. ach unit.
7. Process/Product Detai	ls	
Ma	ximum Anticipated Well(s) Production for Facil	tiy:
Produced Material	Throughput	Units
Gas	750	MMCF/day
Oil	350	barrels/day
Water	10	barrels/day
Other (Specify)		
Maximum An	ticipated Throughput for Principal Product(s) (a	s applicable):
Produced Material	Throughput	Units
Flared Gas	750	MMCF/day
Oil	350	barrels/day
Water	10	barrels/day
Other (Specify)		
8. Zoning		
A. Is the facility (either exist county zoning ordinance Yes	sting or proposed) located in accordance with an es? If no, please explain	y applicable city and/or
	sting or proposed) required to obtain any zoning y at this site? If yes, please explain.	variance to
C. Is the required USGS qu	adrangle map or equivalent attached?	☑ Yes □ No

Facility (Agency Interest) Information

Section OPGP - A

9. MS Secretary of State Registration / Certificate of Good Standing

No permit will be issued to a company that is not authorized to conduct business in Mississippi. If the company applying for the permit is a corporation, limited liability company, a partnership or a business trust, the application package should include proof of registration with the Mississippi Secretary of State and/or a copy of the company's Certificate of Good Standing. The name listed on the permit will include the company name as it is registered with the Mississippi Secretary of State.

It should be noted that for an application submitted in accordance with 11 Miss. Admin. Code Pt. 2, R. 2.8.B. to renew a State Permit to Operate or in accordance with 11 Miss. Admin. Code Pt. 2, R. 6.2.A(1)(c). to renew a Title V Permit to be considered timely and complete, the applicant shall be registered and in good standing with the Mississippi Secretary of State to conduct business in Mississippi.

). Address aı	nd Locat	ion of Facility Records	· · · · · · · · · · · · · · · · · · ·	
Physical Ad	dress			
1. Street Ad	dress:	140 Mayfair Road, Suite 900		
2. City:	Hattiesbu	ırg	3. State:	MS
4. County:	Forrest		5. Zip Code:	39402
6. Telephone	e No.:	601-518-0624	7. Fax No.:	601-450-4448

EMISSIONS EQUIPMENT AT A SYNTHETIC MI	NOR SOURCE
Facility (Agency Interest) Information	Section OPGP - A

11. Certification

The Form must be signed by a Responsible Official as defined in 11 Miss. Admin. Code Pt. 2, R. 2.1.C.(24).

I certify that to the best of my knowledge and belief formed after reasonable inquiry, the statements and information in this application are true, complete, and accurate, and that as a responsible official, my signature shall constitute an agreement that the applicant assumes the responsibility for any alteration, additions, or changes in operation that may be necessary to achieve and maintain compliance with all applicable Rules and Regulations. I am aware that there are significant penalties for submitting false information, including the possibility of fine and imprisonment.

Signature of Responsible Official/DAR	3/3/2025 Date
Adam Barham	3/3/2025
Printed Name	Date

Section B.1: Maximum Uncontrolled Emissions (under normal operating conditions)

Maximum Uncontrolled Emissions are the emissions at maximum capacity and prior to (in the absence of) pollution control, emission-reducing process equipment, or any other emission reduction. Calculate the hourly emissions using the worst case hourly emissions for each pollutant. For each pollutant, calculate the annual emissions as if the facility were operating at maximum plant capacity without pollution controls for 8760 hours per year, unless otherwise approved by the Department. List Hazardous Air Pollutants (HAP) in Section B.3 and GHGs in Section B.4. Emission Point numbering must be consistent throughout the application package and, for existing emission points, should match any MDEQ ID's in the current permit. Fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected. Emissions > 0.01 TPY must be included. Please do not change the column widths on this table.

Emission	TSP ¹	(PM)	PM	-10 ¹	PM-	·2.5¹	S	02	N	Ox	С	0	V	C	TI	S ²	Le	ad	Total	HAPs
Point ID	lb/hr	ton/yr	lb/hr	ten/yr	lb/br	ton/yr	lb/br	ton/yr	lb/br	ton/yr	lb/hr	ton/yr	lb/br	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
AA-001	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	467.72	2048.61	0.00	0.00	0.00	0.00	35.4445	#######
AA-001a	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.02	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.0001	0.0004
AA-002	0.01	0.05	0.02	0.10	0.02	0.10	0.00	0.00	2.70	11.83	4.55	19.91	0.04	0.19	0.00	0.00	0.00	0.00	0.0396	0.1735
AA-002a	0.02	0.07	0.03	0.14	0.03	0.14	0.00	0.00	3.52	15.41	5.92	25.94	0.05	0.21	0.00	0.00	0.00	0.00	0.0516	0.2261
AA-003	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.07	0.30	0.00	0.00	0.00	0.00	0.0031	0.0136
AA-004	Routed to	AA-001																		
AA-005	Routed to	AA-001																		
AA-006	Routed to	AA-001																		
AA-006a	0.00	0.00	0.00	0.02	0.00	0.02	0.00	0.00	0.05	0.21	0.04	0.18	0.00	0.01	0.00	0.00	0.00	0.00	0.0009	0.0041
AA-007	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0,00	0.00	0.02	0.00	0.00	0.00	0.00	0.0043	0.0190
AA-008	Routed to	AA-001																		
AA-009	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0,00	0.00	0.00	0.00	0.00	117.72	12.07	0.00	0.00	0.00	0.00	5.2676	0.5399
AA-010	0.00	0.00	0.00	0.01	0.00	0.01	0.00	0.00	0.01	0.11	0.01	0.09	0.00	0.01	0.00	0.00	0.00	0.00	0.0005	0.0020
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Totals	0.03	0.12	0.06	0.26	0.06	0.26	0.00	0.01	6.28	27.58	10.52	46.12	585.61	2061.41	0.00	0.00	0.00	0.00	40.81	156.23

¹ Condensables: Include condensable particulate matter emissions in particulate matter calculations for PM-10 and PM-2.5, but not for TSP (PM).

² TRS: Total reduced sulfur (TRS) is the sum of the sulfur compounds hydrogen sulfide (H₂S), methyl mercaptan (CH₄S), dimethyl sulfide (C₂H₆S), and dimethyl disulfide (C₂H₆S₂).

Section B.2: Proposed Allowable Emissions

Proposed Allowable Emissions (Potential to Emit) are those emissions the facility is currently permitted to emit as limited by a specific permit requirement or federal/state standard (e.g., a MACT standard); or the emission rate at which the facility proposes to emit considering emissions control devices, restrictions to operating rates/hours, or other requested permit limits that reduce the maximum emission rates. Emission Point numbering must be consistent throughout the application package and, for existing emission points, should match any MDEQ ID's in the current permit. Fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected. Additional columns may be added if there are regulated pollutants (other than HAPs and GHGs) emitted at the facility.

be added if	there are n	egulated p	ollutants (other thar	ı НАРs ал	d GHGs)	emitted at	the facili	y.									
Emission	TS	SP ^I	PM	[10 ¹	PM	2.5 ¹	S	02	N	Ox	C	0	V	C	T	RS	L	ead
Point ID	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/br	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/br	ton/yr	lb/br	ton/yr
AA-001	0.06	0.27	0.25	1.08	0.25	1.08	0.000	0.00	2.24	9.83	10.23	44.80	9.35	40.97	0.00	0.00	0.00	0.00
AA-001a	0.00	0.00	0.00	0.00	0.00	0.00	0.000	0.00	0.00	0.02	0.00	0.02	0.00	0.00	0.00	0.00	0.00	0.00
AA-002	0.01	0.05	0.02	0.104	0.02	0.104	0.001	0.004	2.70	11.83	4.55	19.91	0.04	0.19	0.00	0.00	0.00	0.00
AA-002a	0.02	0.07	0.03	0.135	0.03	0.135	0.00	0.004	3.52	15.41	5.92	25.94	0.05	0.21	0.00	0.00	0.00	0.00
AA-003	0.00	0,00	0,00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.06	0.28	0.00	0.00	0.00	0.00
AA-004	Routed to	AA-001																
AA-005	Routed to	AA-001																
AA-006	Routed to	AA-001																
AA-006a	0.00	0.00	0.00	0.02	0.00	0.02	0.00	0.00	0.05	0.21	0.04	0.18	0.00	0.01	0.00	0.00	0.00	0.00
AA-007	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.02	0,00	0.00	0.00	0.00
AA-008	Routed to	AA-001																
AA-009	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	117.72	12.07	0,00	0.00	0.00	0.00
AA-010	0.00	0.00	0.00	0.01	0.00	0.01	0.00	0.00	0.02	0.11	0.02	0.09	0.00	0.01	0.00	0.00	0.00	0.00
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Totals	0.09	0.39	0.31	1.34	0.31	1.34	0.00	0.01	8,54	37.41	20.76	95.00	127.24	53.75	0.00	0.00	0.00	0.00
T OFFETS	.0.02	1 0.37	0.51	1.54	U.J.	1.34	0,00	0.01	0,54	31,71	20.10	93.00		23.13	V.00	9.00	V.VV	1 0.00

¹ Condensables: Include condensable particulate matter emissions in particulate matter calculations for PM-10 and PM-2.5, but not for TSP (PM).

² TRS: Total reduced sulfur (TRS) is the sum of the sulfur compounds hydrogen sulfide (H₂S), methyl mercaptan (CH₄S), dimethyl sulfide (C₂H₆S), and dimethyl disulfide (C₂H₆S₂).

Section B.3: Proposed Allowable Hazardous Air Pollutants (HAPs)

In the table below, report the Proposed Allowable Emissions (Potential to Emit) for each HAP from each regulated emission unit if the HAP > 0.0001 tpy. Each facility-wide Individual HAP total and the facility-wide Total HAPs shall be the sum of all HAP sources. Use the HAP nomenclature as it appears in the Instructions. Emission Point numbering must be consistent throughout the application package and, for existing emission points, should match any MDEQ ID's in the current permit. For each HAP listed, fill all cells in this table with the emission numbers or a "-" symbol indicates that emissions of this pollutant are not expected or the pollutant is emitted in a quantity less than the threshold amounts described above. Additional columns may be added as necessary to address each HAP.

Emission	Total	HAPs	1,1, tetrachio	2,2 - roethane	1,1,2-trich	loroethane	1,3-bu	tadiene	1,3-dichlo	ropropene	acctalo	dehyde	acro	olein	ben	zene	carbon to	trachloride
Point ID	lb/hr	ton/yr	lb/hr	ton/yr	lb/br	ton/yr	lb/br	ton/yr	lb/br	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/br	ton/yr	lb/hr	ton/yr
AA-001	0.8806	3.1049	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	0.0185	0.0811	<0.0001	<0.0001
AA-001a	0.0001	0.0004	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
AA-002	0.0396	0.1735	<0.0001	0.0001	<0.0001	0.0001	0.0008	0.0035	<0.0001	0.0001	0.0034	0.0149	0.0032	0.0141	0.0019	0.0085	<0.0001	0.0001
AA-002a	0.0516	0.2261	<0.0001	0.0002	<0.0001	0.0001	0.0011	0.0046	<0.0001	0.0001	0,0044	0.0195	0.0042	0.0183	0.0025	0.0110	<0.0001	0,0001
AA-003	0.0036	0.0136	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	0.0005	0.0022	<0.0001	<0.0001
AA-004	Routed to	AA-001																
AA-005	Routed to	AA-001																
AA-006	Routed to	AA-001																
AA-006a	0.0009	0.0041	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
AA-007	0.0043	0.0190	⊲ 0.0001	⊲0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	< 0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
AA-008	Routed to	AA-001																
AA-009	5.2676	0.5399	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	0.5648	0.0579	<0.0001	<0.0001
AA-010	0.00047	0.00205	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
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Totals:	6.2489	4.0836	0.0000	0.0003	0.0000	0.0002	0.0019	0.0082	0.0000	0.0002	0.0079	0.0344	0.0074	0.0324	0.5883	0.1607	0.0000	0.0002

Section B.3: Proposed Allowable Hazardous Air Pollutants (HAPs)

In the table below, report the Proposed Allowable Emissions (Potential to Emit) for each HAP from each regulated emission unit if the HAP > 0.0001 tpy. Each facility-wide Individual HAP total and the facility-wide Total HAPs shall be the sum of all HAP sources. Use the HAP nomenclature as it appears in the Instructions. Emission Point numbering must be consistent throughout the application package and, for existing emission points, should match any MDEQ ID's in the current permit. For each HAP listed, fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected or the pollutant is emitted in a quantity less than the threshold amounts described above. Additional columns may be added as necessary to address each HAP.

Emission	Total	HAPs	chlorot	enzene	chion	oform	ethylbo	nzene	ethylene (dibromide	formal	dehyde	metl	lonze	methylen	e chloride	naphi	halene
Point ID	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	ib/br	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/br	ton/yr
AA-001	0.1414	3.1049	<0.0001	<0.0001	<0.0001	<0.0001	0.0014	0.0061	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
AA-001a	0.0001	0.0004	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
AA-002	0.0396	0.1735	<0.0001	0.0001	<0.0001	0.0001	<0.0001	0.0001	<0.0001	0.0001	0.0250	0.1097	0.0037	0.0164	0.0001	0.0002	0.0001	0.0005
AA-002a	0.0227	0.2261	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	0.0002	<0.0001	0.0001	0.0326	0.1430	0.0049	0,0213	<0.0001	0.0003	0.0002	0.0007
AA-003	0.0031	0.0136	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	0.0002	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
AA-004	Routed to	AA-001															<0.0001	<0.0001
AA-005	Routed to	AA-001															<0.0001	<0.0001
AA-006	Routed to	AA-001															<0.0001	<0.0001
AA-006a	0.0009	0.0041	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	0.0002	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
AA-007	0.0043	0.0190	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
AA-008	Routed to	AA-001															<0.0001	<0.0001
AA-009	5.2676	0.5399	<0.0001	<0.0001	<0.0001	<0.0001	0.0216	0.0022	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0,0001	<0.0001	<0.0001
AA-010	0.0005	0.0020	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
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Totals:	5.4802	4.0836	0.0000	0.0001	0.0000	0.0001	0.0230	0.0088	0.0000	0.0003	0.0577	0.2529	0.0086	0.0377	0.0001	0.0005	0.0003	0.0012

Section B.3: Proposed Allowable Hazardous Air Pollutants (HAPs)

In the table below, report the Proposed Allowable Emissions (Potential to Emit) for each HAP from each regulated emission unit if the HAP > 0.0001 tpy. Each facility-wide Individual HAP total and the facility-wide Total HAPs shall be the sum of all HAP sources. Use the HAP nomenclature as it appears in the Instructions. Emission Point numbering must be consistent throughout the application package and, for existing emission points, should match any MDEQ ID's in the current permit. For each HAP listed, fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected or the pollutant is emitted in a quantity less than the threshold amounts described above. Additional columns may be added as necessary to address each HAP.

Emission	Total	HAPs	Ρ/	VH.	styr	ene	tolu	ene	vinyl c	hloride	xy:l	lene	bes	anc	PC	M		
Point ID	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/br	ton/yr	lb/hr	ton/yr
AA-001	0.1414	3.1049	<0.0001	<0.0001	<0.0001	<0.0001	0.0151	0.0661	<0.0001	<0.0001	0.0080	0.0352	0.6659	2.9165	<0.0001	<0.0001		
AA-001a	0.0001	0.0004	< 0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	0.0001	0.0004	<0.0001	<0.0001		
AA-002	0.0396	0.1735	0.0002	0.0008	<0.0001	0.0001	0.0007	0.0030	<0.0001	<0.0001	0.0002	0.0010	<0.0001	<0.0001	<0.0001	<0.0001		
AA-002a	0.0227	0.2261	0.0002	0.0010	<0.0001	<0.0001	0.0009	0.0039	<0.0001	<0.0001	0.0003	0.0014	<0.0001	<0.0001	<0.0001	<0.0001		
AA-003	0.0031	0.0136	<0.0001	<0.0001	<0.0001	<0.0001	0.0004	0.0017	<0.0001	<0.0001	0.0002	0.0009	0.0206	0.0902	<0.0001	<0.0001		
AA-004	Routed to	AA-001																
AA-005	Routed to	AA-001																
AA-006	Routed to	AA-001																
AA-006a	0.0009	0.0041	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	0.0009	0.0039	<0.0001	0.0001		
AA-007	0.0043	0.0190	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001		
AA-008	Routed to	AA-001																
AA-009	<0.0001	0.5399	<0.0001	<0.0001	40.0001	<0.0001	0.5593	0.0573	<0.0001	<0.0001	0.2946	0.0302	3.8273	0.3923	<0.0001	<0.0001		
AA-010	0.00047	0.00205	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	0.00044	0.00193	<0.0001	<0.0001		
											_							\vdash
	-											_						
				-							_							├ ──
																		<u> </u>
Totals:	0.2126	4.0836	0.0004	0.0017	0.0000	0.0001	0.5763	0.1320	0.0000	0.0000	0.3034	0.0687	4.5152	3.4052	0.0000	0.0001		

Section B.4: Greenhouse Gas Emissions

Applicants must report potential emission rates in SHORT TONS per year, as opposed to metric tons required by Part 98. Emission Point numbering must be consistent throughout the

		CO ₂ (non- biogenic) ton/yr	CO ₂ (biogenic) ² ton/yr	N₂O ton/yr	CH ₄ ton/yr	SF ₆ ton/yr	PFC/HFC ³ ton/yr					Total GHG Mass Basis ton/yr ⁵	Total CO ₂ e ton/yr ⁶
Emission Point ID	GWPs 1	1	1	298	25	22,800	footnote 4						
AA-001	mass GHG	18426.95	0	0.03	62.49	0	0					18489.47	N/A
AA-001	CO2e	18426.95	0	8.93	1562.19	0	0				1	N/A	19998.07
AA-001a	mass GHG	25.59	0	0.00	0.00	0	0					25.59	N/A
AA-0018	CO2e	25.59	0	0.01	0.01	0	0					N/A	25.62
AA-002	mass GHG	624.23	0	0.00	0.01	0	0					624.24	N/A
AA-002	CO2e	624.23	0	0.35	0.29	0	0					N/A	624.88
AA-002a	mass GHG	813.39	0	0.00	0.02	0	0					813.41	N/A
AA-0028	CO2e	813.39	0	0.46	0.38	0	0					N/A	814.23
AA-003	mass GHG	0.04	0	0.00	0.27	0	0					0.32	N/A
AA-003	CO2e	0.04	0	0.00	6.81	0	0					N/A	6.85
AA-004	mass GHG	0	0	0	0	0	0					0.00	N/A
AA-004	CO2e	0	0	0	0	0	0					N/A	0.00
AA-005	mass GHG	0	0	0	0	0	0					0.00	N/A
AA-005	CO2e	0	0	0	0	0	0					N/A	0.00
AA-006	mass GHG	0	0	0	0	Ó	0					0.00	N/A
AA-000	CO ₂ e	0	0	0	0	0	0					N/A	0.00
A A .00C-	mass GHG	255.45	0	0.00	0.00	0	0					255.46	N/A
AA-006a	COze	255.45	0	0.14	0.12	.0	0			1		N/A	255.71
4 4 400	mass GHG	0	0	0	0	Ö	O .					0.00	N/A
AA-007	CO ₂ e	0	0	0	0	0	0					N/A	0.00
1 1 000	mass GHG	0	0	0	0	0	0			1	1	0.00	N/A
AA-008	COze	0	0	0	0	0	0					N/A	0.00
4.4.000	mass GHG	0.03	0	0	0.18	0	0					0.21	N/A
AA-009	CO ₂ e	0.03	0	0	4.50	0	0					N/A	4.53
4 4 040	mass GHG	127.73	0	0.00	0.00	0	. 0				1 1	127.73	N/A
AA-010	COze	127.73	0	0.07	0,06	0	0				1 1	N/A	127.86
FACILITY	mass GHG	20145.70	0	0.49	63.34	0.00	0.00	i		i i	1 i	20209.53	N/A
TOTAL	CO ₂ e	20145.70	0	145,67	1583.51	0.00	0.00	0.5	—	 	 	N/A	21874.88

¹ GWP (Global Warming Potential): Applicants must use the most current GWPs codified in Table A-1 of 40 CFR part 98. GWPs are subject to change, therefore, applicants need to check 40 CFR 98 to confirm GWP values.

² Biogenic CO2 is defined as carbon dioxide emissions resulting from the combustion or decomposition of non-fossilized and biodegradable organic material originating from plants, animals, or

micro-organisms.

For HFCs or PFCs describe the specific HFC or PFC compound and use a separate column for each individual compound.

⁴ For each new compound, enter the appropriate GWP for each HFC or PFC compound from Table A-1 in 40 CFR 98.

⁵ Greenhouse gas emissions on a mass basis is the ton per year greenhouse gas emission before adjustment with its GWP. Do not include biogenic CO₂ in this total.

⁶ CO₂e means Carbon Dioxide Equivalent and is calculated by multiplying the TPY mass emissions of the greenhouse gas by its GWP. Do not include biogenic CO₂e in this total.

Section B.5: Stack Parameters and Exit Conditions

Emission Point numbering must be consistent throughout the application package and, for existing emission points, should match any MDEQ ID's in the current permit.

Emission Point ID	Horizontal		Height Above Ground	Base Elevation	Exit Temp.	Inside Diameter or Dimensions	Velocity	Moisture by Volume	Geographic Position (degrees/minutes/seconds)	
rount 1D	V=Vertical)	(Yes or No)	(ft)	(ft)	(°F)	(ft)	(ft/sec)	(%)	Latitude	Longitude
AA-001	Н	No	40	415	1800	0.50	100	TBD	31/51/7.848N	89/19/7.464W
AA-002	Н	Yes	7	415	TBD	TBD	TBD	TBD	31/51/7.848N	89/19/7.464W
AA-002a	Н	yes	7	415	TBD	TBD	TBD	TBD	31/51/7.848N	89/19/7.464W
AA-003	N/A-Fugitives	N/A	N/A	415	N/A	N/A	N/A	N/A	31/51/7.848N	89/19/7.464W
AA-004	N/A-Separator	N/A	N/A	415	N/A	N/A	N/A	N/A	31/51/7.848N	89/19/7.464W
AA-005	N/A-Separator	N/A	N/A	415	N/A	N/A	N/A	N/A	31/51/7.848N	89/19/7.464W
AA-006	N/A-Heater Treater	N/A	N/A	415	N/A	N/A	N/A	N/A	31/51/7.848N	89/19/7.464W
AA-006a	TBD	TBD	TBD	415	TBD	TBD	TBD	TBD	31/51/7.848N	89/19/7.464W
AA-007	N/A-Tanks	N/A	N/A	415	N/A	N/A	N/A	N/A	31/51/7.848N	89/19/7.464W
AA-008	N/A-Tanks	N/A	N/A	415	N/A	N/A	N/A	N/A	31/51/7.848N	89/19/7.464W
AA-009	N/A-Truck Loading	N/A	N/A	415	N/A	N/A	N/A	N/A	31/51/7.848N	89/19/7.464W
AA-010	TBD	TBD	TBD	415	N/A	TBD	TBD	TBD	31/51/7.848N	89/19/7.464W

¹ A WAAS-capable GPS receiver should be used and in the WGS84 or NAD83 coordinate system.

						· · · · · · · · · · · · · · · · · · ·		<u> </u>							
Fue	I Bu	rning E	Equipment –	- Internal C	Combusti	ion	Section	n OPGP-	n						
Eng	gines	3					Section	n Oi Gi -	D						
1.	Em	ission Po	int Description	on											
	A.	Emission P	oint Designation (Re	ef. No.): AA-0	02a										
			_ ,						_						
	B.	Equipment	Description (includ	ing serial number)	: 215 HP RIC	CE for sales gas	s compresso	r							
									_						
	C.	Manufactur	Manufacturer: Caterpillar D. Date of Manufacture 2011 and Model No.:												
		and Model No.:													
	E.	Maximum Heat Input (higher heating value): 1.59 MMBtu/hr													
	F.	Rated Power	er: 215	hp	162	kW									
	G.	Is the engin	e an EPA-certified	engine?	No	Yes or No									
		T.T	N												
	H.	Use:	Non-emerger	icy	∐ Emei	rgency									
	I.	Displaceme	ent per cylinder:		, \sqcap	10 to <30 Lite	rs 🗆	≥ 30 Liters							
	••	Displaceme	nic per cylinder.	Z TO Ditor.	, L	TO TO SO DITO		j _ 50 Liters							
	J.	Engine Igni	ition Type:		ion	☐ Compres	sion Ignition	1							
			7.				3								
	K.	Engine Bur	n Type:	4-stroke	2-strok	e 🛛	Rich Burn	Lean	Burn						
		(check all ti	hat apply)												
			_		_										
	L.	Status:		Operating	Propose	ed 📙	Under								
	M	Data of com		- 4 :	1:6::	(f C									
	M.		struction, reconstrueurces) or date of anti			n (for Coi	nstruction								
		J	,	•			3/2025								
2.	Fue	el Type													
	Com	plete the follo	owing table, identify	ing each type of fi	uel and the am	ount used. Spe	cify units of	measurement.	•						
	FU	EL TYPE	HEAT	% SULFUR	% ASH	MAXIMU		MAXIMUM	7						
			CONTENT			HOURLY US	SAGE YE	EARLY USAGE	,						
		Nat.	1020 BTU/Ft3	0.00004	0.0	1.59 MC	F	13.93 MMCF							
	Gas	s/propane			1				\dashv						
									\dashv						
									\dashv						
	<u> </u>				1 .	I									

Compliance Plan Section OPGP-G

Part 1. Equipment List

List all equipment and the corresponding federal and/or state regulation that is applicable. Clearly identify federal regulations from state requirements. Provide the expected or actual construction date, startup date and removal date if the equipment is no longer on site.

EMISSION UNIT (Ref No.)	FEDERAL or STATE REGULATION Ex. 40 CFR Part, Subpart Ex. 11 Miss. Admin. Code Pt. 2, R. 1.4.B(2).	CONSTRUCTION DATE	STARTUP DATE	REMOVAL DATE
Example: Engines	40 CFR 63, Subpart ZZZZ	10/01/2002	11/15/2019	N/A
Example: Fugitive Emissions	40 CFR 60, Subpart OOOOa	10/01/2019	11/15/2019	N/A
Example: Flare	11 Miss. Admin. Code Pt. 2, R.1.4.B(2).	12/01/2019	12/02/2019	N/A
This list of exam should be comp	mples is not intended to be conclusive for each type of emission source. Th oleted.	is list only provides e.	xamples of ho	w the table
AA-001 Flare and facility wide	11 Miss. Admin. Code Pt. 2, R.1.4.B(2).			
AA-002	40 CFR 63, Subpart ZZZZ			
AA-002, AA- 010	11 Miss. Admin. Code Pt. 2, R.1.3.B.			
AA-002, ,AA- 006a, AA-010	11 Miss. Admin. Code Pt. 2, R.1.3.D(1)(a).			
AA-003 Fugitive Emissions	40 CFR 60, Subpart OOOOa			

ATTACHMENT A

Calculations for Venture Stone 9-5 No. 1 Tank Battery

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Site Information for Calculations

Site Name: Stone 9-5 No. 1 Tank Battery

 Potential Crude Production
 78,840 bbl/yr
 bbl/yr

 Potential Gas production
 219,000 mcf/yr

 Potential Produced Water
 3,650 bbl/yr

 Initial Crude Production
 216 bbl/day
 (expected maximum daily production)

 Initial Gas Production
 750 mcf/day
 (expected maximum daily production)

 Initial Water Production
 10 bbl/day
 (expected maximum daily production)

Crude Gravity 49

Oil tank W&B Losses

1.31 SCF/stock tank bbl (estimated using E&P Tanks)
Oil tank Flash Gas

1.887 SCF/stock tank bbl (estimated using E&P Tanks)
Water tank W&B Losses

0.0131 SCF/stock tank bbl (using 1% of oil tank emissions)
Water tankFlash Gas

0.1887 SCF/stock tank bbl (using 1% of oil tank emissions)

VRU recovery efficiency 0.00% Flare destruction efficiency 98.00%

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Emission Point Summary

Emission Point Number	Emission Point Description	Design Capacity	Units	Operating Hours	
AA-001	Flare	10.25	MMBtu/hr	8760	
AA-001a	Flare Pilot	0.05	MMBtu/hr	8760	
AA-002	Power Oil Pump Engine	165	hp	8760	
AA-002a	Compressor Engine	150	hp	8760	
AA-003	Fugitive emissions- equipment leaks	-	-	8760	
AA-004	High Pressure Separator -		-	8760	
AA-005	Low Pressure Separator		-	8760	
AA-006	Heater Treater		-	8760	
AA-006a	Heater Treater (burner)	0.5	mmBtu/hr	8760	
AA-007	Misc. Chemical Tanks	. a .i	-	8760	
AA-008	Oil and Water Storage Tanks		-	8760	
AA-009	Truck Loading	16,000	gal/hr	As needed	
AA-010	Line Heater	0.25	mmBtu/hr	8760	

Note: Storage tanks, separators, and heater treater vent to the flare.

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Proposed Annual Emissions, controlled

Emission	1-	Annual Emissions, tpy								GHG Emissions, tpy			
CURID Funssion	Emission Unit	PM	PM10	PNI2.5	VOC	NOx	CO	SO2	Total	'CO2	CH4	N2O	GO2e
AA-001	Flare	0.27	0.27	0.27	40.97	9.83	44.80	0.00	3.1049	18426.95	62.49	0.03	19998.07
AA-001a	Flare Pilot	0.00	0.00	0.00	0.00	0.02	0.02	0.00	0.0004	25.59	0.00	0.00	25.62
AA-002	Power Oil Pump Engine	0.051	0.104	0.104	0.16	11.83	19.91	0.003	0.1735	624.23	0.03	0.00	625.26
AA-002a	Compressor Engine	0.066	0.135	0.135	0.09	6.78	25.94	0.002	0.2261	813.39	0.01	0.00	814.14
AA-003	Fugitive emissions- equipment leaks	-	-	-	0.30	-	-		0.0136	0.04	0.02	0.00	0.43
AA-004	High Pressure Separator		Gas	routed to	Flare			•	•				•
AA-005	Low Pressure Separator		Gas	routed to	Flare								
AA-006	Heater Treater		Gas	routed to	Flare								
AA-006a	Heater Treater (burner)	0.00408	0.01632	0.01632	0.01181	0.21471	0.18035	0.00129	0.0041	255.45	0.00	0.00	255.71
AA-007	Misc. Chemical Tanks (4)	-	-	-	0.02	-	-	-	0.0190			-	
AA-008	Oil and Water Tanks (4)		Gas	routed to	flare							•	•
AA-009	Truck Loading				12.07				0.5399	0.03	0.18	0	4.49
AA-010	Line Heater	0.00204	0.00816	0.00816	0.01	0.10735	0.09018	0.00064	0.0020	127.73	0.00	0.00	127.86
	Totals	(0:39	0.53	0,53	53.62	28,67	80.84	0,01	4:0815	20145,70	62/73	0.03	21723,72

Notes

Storage tanks emissions are included in flare emissions.

Potential Annual Emissions, uncontrolled

Emission			Annual Emissions, tpy							mary y	GHG Em	issions, tpy	
UnitiD	Émission Unit	PM	PM10,	PM2.5	VOC	NOx	(CO	S02	Total HAPs	CO2	CH4	N2O	CO2e
AA-001	Facility gas emissions		-	-	2048.61	-	•	•	155.25	465.40	3125.06	0.00	78591.84
AA-002	Power Oil Pump Engine	0.051	0.104	0.104	0.16	11.83	19.91	0.003	0.17	624.23	0.01	0.00	624.88
AA-002a	Compressor Engine	0.066	0.135	0.135	0.21	15.41	25.94	0.004	0.23	813.39	0.02	0.00	814.23
AA-003	Fugitive emissions- equipment leaks	-		-	0.30	-			0.01	0.04	0.27	0.00	6.85
AA-004	High Pressure Separator		Gas	routed to	Flare								
AA-005	Low Pressure Separator		Gas	routed to	Flare								
AA-006	Heater Treater		Gas	routed to	Flare								
AA-006a	Heater Treater (burner)	0.00	0.02	0.02	0.01	0.21	0.18	0.00	0.0041	232.23	0.00	0.00	232.47
AA-007	Misc. Chemical Tanks	-	-	-	0.02	-	-	-	0.02	-	•		•
AA-008	Oil and Water Storage Tanks		Gas	routed to	flare								
AA-009	Truck Loading				12.07				0.5399	0.03	0.18	0	4.49
AA-010	Line Heater	0.00	0.01	0.01	0.01	0.11	0.09	0.00	0.0020	127.73	0.00	0.00	127.86
	Totals	0.12	0.28	0.26	2061:37	27.45	46,03	-0.01	158.22	2135:32	3126:54	(0.00	80274.76

Notes:

Storage tanks emissions are included in flare emissions, AA-001.

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Facility Maximum Hourly Emissions, Controlled

Emission		PARKY.	Emissions; lb/hr								GHG Emis	slons, lb/hr	T.
UnitiD	Émission Unit	PM	PM10	PM2:5	VOC	NOx	CO	SO2	Total HAPs	GO2	CH4	N2O	CO2e
AA-001	Flare	0.06	0.06	0.08	9.35	2.24	10.23	0.00	0.88	4207.07	14.27	0.01	4565.77
AA-001a	Flare Pilot	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	5.84	0.00	0.00	5.85
AA-002	Power Oil Pump Engine	0.01	0.02	0.02	0.04	2.70	4.55	0.00	0.04	142.52	0.01	0.00	142.75
AA-002a	Compressor Engine	0.02	0.03	0.03	0.05	3.52	5.92	0.00	0.05	185.71	0.00	0.00	185.90
AA-003	Fugitive emissions- equipment leaks	-	-		0.07	-		-	0.00	0.01	0.00	0.00	0.10
AA-004	High Pressure Separator				GAS ROU	TED TO FL	ARE					-	
AA-005	Low Pressure Separator				GAS ROU	TED TO FL	ARE						
AA-006	Heater Treater				GAS ROU	TED TO FL	ARE						
AA-006a	Heater Treater (burner)	0.00	0.00	0.00	0.00	0.05	0.04	0.00	0.00	58.32	0.00	0.00	58.38
AA-007	Misc. Chemical Tanks	-	-		0.00	-	•	•	0.00	-	-	-	0.00
AA-008	Oil and Water Storage Tanks		GAS ROUTED TO FLARE										
AA-009	Truck Loading	-	-		117.72	-	-	-	5.27	0.01	0.04	0	1.03
AA-010	Line Heater	0.00	0.00	0.00	0.00	0.02	0.02	0.00	0.0005	29.16	0.00	0.00	29.19
	Totals	0,09	0.12	0.12	127.23	8/52	20.74	0.002	6.25	4899,47	14.32	0,01	4959:77

Notes

Storage tanks emissions are included in flare emissions.

Truck loading hourly emissions are dictated by the capacity of the transfer pump

4.38 tpy = 1 PPH

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Flash Gas Analysis and Conversions

Component	VOC and/or HAP?	Moi %	Wt%
Total S	None	***	0.00000%
CO2	None	0.362%	0.160%
N2	None	0.000%	0.000%
Methane	None	11.546%	1.852%
Ethane	None	6.480%	1.949%
Propane	VOC	19.755%	8.712%
Isobutane	VOC	20.171%	11.724%
Butane	VOC	12.576%	7.309%
Isopentane	VOC	9.194%	6.633%
Pentane	VOC	5.953%	4.295%
Hexane	VOC	3.906%	3.366%
Heptanes	VOC	6.630%	6.644%
Benzene	VOC and HAP	0.390%	0.544%
Toluene	VOC and HAP	0.388%	0.639%
e-Benzene	VOC and HAP	0.015%	0.028%
Xylenes	VOC and HAP	0.211%	0.400%
n-hexane	VOC and HAP	2.422%	3.726%
Total VOC		79.190%	54.020%
Total HAP		3.426%	5.337%

Heat of combustion, Btu/ft ³	2465.9
Molecular weight	46.02

Gas analysis generated by E&P Tanks software.

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Produced Gas Analysis and Conversions

Component	VOC and/or HAP?	Mol %	Wt %
Total S	None	0.000%	0.00000%
CO2	None	3.663%	6.696%
N2	None	2.039%	2.372%
Methane	None	67.467%	44.953%
Ethane	None	13.830%	17.272%
Propane	voc	7.074%	12.956%
isobutane	VOC	1.484%	3.582%
Butane	VOC	2.649%	6.395%
Isopentane	VOC	0.623%	1.867%
Pentane	VOC	0.554%	1.660%
Hexane	VOC	0.573%	2.051%
n-Hexane	VOC and HAP	0.136%	0.196%
Heptanes+	voc	0.044%	0.196%
Benzene	VOC and HAP	0.042%	0.051%
Toluene	VOC and HAP	0.010%	0.039%
e-Benzene	VOC and HAP	0.001%	0.004%
Xylenes	VOC and HAP	0.007%	0.020%
Total VOC		13.001%	28.707%
Total HAP		0.196%	0.310%

Heat of combustion, Btu/ft ³	1302.0
Molecular weight	24.08

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TANK W & B GAS COMPOSITION

Component	VOC and/or HAP?	Mol %	Wt %			
Total S	None	0.000%	0.00000%			
CO2	None	0.32%	0.25%	44.1	0.140414	
N2	None	0.00%	0.00%	28.01	0	
Methane	None	4.76%	1.35%	16.04	0.762878	
Ethane	None	7.23%	3.86%	30.07	2.174783	
Propane	VOC	24.31%	19.03%	44.1	10.72005	
Isobutane	VOC	23.60%	24.34%	58.12	13.71649	
Butane	VOC	14.17%	14.62%	58.12	8.235546	
Isopentane	VOC	9.38%	12.01%	72.15	6.766083	
Pentane	VOC	5.77%	7.39%	72.15	4.163055	
Hexane	VOC	3.28%	5.02%	86.18	2.8286	
Heptanes+	VOC	4.52%	8.03%	100.21	4.526586	
Benzene	VOC and HAP	0.32%	0.44%	78.11	0.247531	0.539932
Toluene	VOC and HAP	0.27%	0.44%	92.14	0.245092	
e-Benzene	VOC and HAP	0.01%	0.02%	106.17	0.009449	
Xylenes	VOC and HAP	0.12%	0.23%	106.16	0.129091	
n-hexane		1.95%	2.98%	86.18	1.677235	
Total VOC		85.75%	91.56%	I	56.34289	
Total HAP		2.660%	4.10%			

Heat of combustion, Btu/ft³ 2796.8 Molecular weight 51.43

Note: W&B vapors and truck loading vapors assumed to have same composition Gas analysis generated by E&P Tanks software.

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Tank Uncontrolled Emissions Summary

			initiai		
	<u>Potential</u>		Production		
Total flash gas ,	1,488,400	SCF/yr	170	SCF/hr	
Total flash gas ,	88.43	tpy	20.19	lb/hr	
Total tank W&B loss	103,328	SCF/yr	12	SCF/hr	
Total tank W &B losses	6.86	tpy	1.57	lb/hr	
Total tank emissions	95.29	tpy	21.76	lb/hr	
Tank emissions to flare	95.29	tpy	21.76	lb/hr	
	688.76				
	0.04	0.04	0.0001		

Notes:

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^{1.} Total flash gas calculated using gas/oil ratio from E&P tanks program and potential crude and water production

^{2.} All tank emissions included with flare, Emission Point AA-001.

Calculation of Criteria and Hazardous Flare Emissions Using 30-day Average Production Values

Detential

Gas Flow to Flare:

		<u>Potentiai</u>
Flow to flare of tank flash gas	=	88.43 tpy
Flow to flare of tank W&B emissions		6.86 tpy
flow to flare from truck loading	=	0.00 tpy
Total process gas to flare	=	95.29 tpy
Produced gas to flare	=	6947.98 tpy
	=	219000.00 mcf/yr

Produced gas combustion heat = 285138.00 MMBtu/yr process gas combustion heat = 3875.34 MMBtu/yr flare gas combustion heat, total = 289013.34 MMBtu/yr

			<u>Potentia</u>	<u>l Emissions</u>		Potential Er	<u>missions</u>
	<u>Pollutant</u>	Emission factor, lbs/MMBtu	<u>lb/hr</u>	<u>tpy</u>	<u>Pollutant</u>	<u>lb/hr</u>	<u>tpy</u>
	NOx	0.068	2.243	9.826	n-hexane	0.6659	2.9165
Calculation	n CO	0.31	10.228	44.797	benzene	0.0185	0.0811
	PM	0.00186	0.001	0.269	e-benzene	0.0014	0.0061
	VOC	mass balance	9.354	40.972	toluene	0.0151	0.0661
	SO ₂	mass balance	0.000	0.000	xylenes	0.0080	0.0352
	PM10/PM2.5	0.00745	0.246	1.077	Total HAPs	0.7089	3.1049

Notes:

- 1. Emission factors from AP-42, Table 13.5-1, are used to calculate NOx and CO emissions, and PM emission factor from AP-42, Table 1.4-2.
- Mass balance calculations utilize flare input gas flow and a flare destruction efficiency of 98% minimum.
- 3. Mass balance for sulfur assumes all sulfur converted to SO2 in flare.

ank Battery HAP emissions calculated using mass balance and 98% destruction efficiency Oil General Permit Coverage Application

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Calculation of Maximum Hourly Criteria and Hazardous Flare Emissions Using Initial Production Values

Gas Flow to Flare:

	<u>Potential</u>
=	20.19 lbs/hr
	1.57 lbs/hr
=	0.00 lbs/hr
=	21.76 lbs/hr
=	1982.87 lbs/hr
=	31.25 mcf/hr
=	40.69 MMBtu/hr
=	0.44 MMBtu/hr
=	41.13 MMBtu/hr
	= = = =

			Maximum Hourly Emissions		Potential Emissions
	<u>Pollutant</u>	Emission factor, Ibs/MMBtu	<u>lb/hr</u>	<u>Pollutant</u>	<u>lb/hr</u>
	NOx	0.068	2.797	n-hexane	0.8285
Calculation	CO	0.37	15.218	benzene	0.0226
	PM	0.00745	0.306	e-benzene	0.0017
	VOC	mass balance	11.631	toluene	0.0182
	SO ₂	mass balance	0.000	xylenes	0.0096
				Total HAPs	0.8806

Notes:

- Emission factors from AP-42, Table 13.5-1, are used to calculate NOx and CO emissions, and PM emission factor from AP-42, Table 1.4-2.
- 2. Mass balance calculations utilize flare input process gas flow and a flare destruction efficiency of 98% minimum.
- 3. Mass balance for sulfur assumes all sulfur converted to SO2 in flare.
- 4. HAP emissions calculated using mass balance and 98% destruction efficiency

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Calculation of Uncontrolled Emissions of Produced Gas

		<u>Potential</u>
Flow to flare from tank flash gas	=	88.43 tpy
Flow to flare from tank W&B emissions	=	6.86
flow to flare from truck loading	=	0.00 tpy
Produced gas to flare from separators	=	6947.98 tpy

		Potential I	<u>Emissions</u>
<u>Pollutant</u>	Emission factor, lbs/MMBtu	<u>lb/hr</u>	tpy
VOC	mass balance	467.719	2048.61
H2S	mass balance	0.000	0.00
n-hexane	mass balance	33.293	145.82
benzene	mass balance	0.926	4.06
e-benzene	mass balance	0.069	0.30
toluene	mass balance	0.754	3.30
Calculation xylenes	mass balance	0.402	1.76
total HAPs	mass balance	35.444	155.25
methane	mass balance	713.484	3125.06
CO2	mass balance	106.255	465.40

Note: For calculation of uncontrolled emissions, flare efficiency is 0%.

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Calculation of Flare GHG Emissions

Process gas to flare, mmcf/yr 1.57
N2O emission factor, kg/mmBtu 0.0001
HHV, mmBtu/scf 0.001235
CO2 density, kg/ft3 0.052600
CH4 density, kg/ft3 0.019200
flare efficiency 98.00%

PROCESS GAS

carbon	CO2 (from c	combustion)	CO2 input	СН4, илсо	mbusted	N2O	CO2e
atoms	cubic ft.	tpy	tpy	cubic ft.	tpy¹	tpy ¹	tpy
			3.29E-01	3.63E+03	7.66E-02	2.13E-04	2.31E+00
1	1.78E+05	1.03E+01	*	ł			1.03E+01
2	2.00E+05	1.15E+01		:			1.15E+01
3	9.13E+05	5.28E+01					5.28E+01
4	2.02E+06	1.17E+02					1.17E+02
5+	2.06E+06	1.19E+02					1.19E+02
Total	5.36E+06	3.10E+02	3.29E-01	3.63E+03	7.66E-02	2.13E-04	3.13E+02

PRODUCED GAS

produced gas to flare, mmcf/yr

219.00

carbon	CO2 (from c	ombustion)	CO2 input	CH4, unco	mbusted	N2O	CO2e
atoms	cubic ft.	tpy	tpy	cubic ft. tpy		tpy	tpy
			4.64E+02	2.96E+06	6.24E+01	2.98E-02	2.03E+03
1	1.45E+08	8.38E+03					8.38E+03
2	5.94E+07	3.43E+03					3.43E+03
3	4.55E+07	2.64E+03					2.64E+03
4	3.55E+07	2.05E+03					2.05E+03
5+	1.99E+07	1.15E+03					1.15E+03
Total	3.05E+08	1.77E+04	4.64E+02	2.96E+06	6.24E+01	2.98E-02	1.97E+04

Note: GHG emissions calculated using procedures from 40 CFR 98.233(n)(4)

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Equipment Component Fugitive Emissions

Components	Counts	Emission Factor ¹	Emissions	Wt. Fraction	VOC Em	issions	VOC%	HAP Em	issions	GHG I	Emissions, t	on/yr
		scf/hr/component	lbs/hr	voc	lb/hr	tpy	HAP ³	lb/hr	tpy	CO2	CH4	CO2e
Valves:	37								7			
gas/vapor	24	0.027	0.041116838	0.29	0.012	0.05	0.31%	0.000	0.001	0.012035	0.080884	2.03
light oil ²	13	0.05	0.041243742	0.54	0.022	0.10	5.34%	0.002	0.010	0.012073	0.073758	1.86
heavy oil	0	0.0005	0	0.29	0.000	0.00	0.31%	0.000	0.000	0	0	0.00
Pumps:			0	0.29			0.31%	0.000	0.000	0	0	0.00
Light oil	0	0.01	0	0.73	0.000	0.00	1.66%	0.000	0.000	0	0	0.00
heavy oil	0	0	0	0.29			0.31%	0.000	0.000	0	0	0.00
Flanges:	46		0	0.29			0.31%	0.000	0.000	0	0	0.00
gas/vapor		0	0	0.29	0.000	0.00	0.31%	0.000	0.000	0	0	0.00
light oil	46	0.003	0.008756364	0.73	0.006	0.03	1.66%	0.000	0.001	0.002563	0.015659	0.39
heavy oil	0	0.0009	0	0.29	0.000	0.00	0.31%	0.000	0.000	0	0	0.00
Relief Valve:			0	0.29			0.31%	0.000	0.000	0	0	0.00
gas/vapor	4	0.04	0.010152306	0.29	0.003	0.01	0.31%	0.000	0.000	0.002972	0.018156	0.46
Connectors:	101		0	0.29			0.31%	0.000	0.000	0	0	0.00
gas/vapor	67	0.003	0.012753834	0.29	0.004	0.02	0.31%	0.000	0.000	0.003733	0.022808	0.57
light oil	34	0.007	0.015101555	0.73	0.011	0.05	1.66%	0.000	0.001	0.00442	0.027007	0.68
heavy oil	0	0.0003	0	0.29	0.000	0.02	0.31%	0.000	0.000	0	0	0.00
Other	1	0.3	0.019035573	0.29	0.005	0.02	1.66%	0.000	0.001	0.005572	0.034042	0.86
				Totals	0.064	0.302		0.003	0.014	0.043	0.272	6.851

Notes:

1. Emission factors and equipment counts taken from 40 CFR 98, subpart W.

Light oil is defined as having Al	PI gravity greater than or e	qual to 20 degrees	API.	Equipment	Count	Valves	Flan	ges Fitt	ings <u>prv</u>	Other	
Vapors emitted from gas service	e equipment assumed to be	e same as produce	ed gas,	wellhead		1	5	10	4	0	1
vapor from liquid service equip	ment assumed to be the sa	ame as flash gas.		heater treater		1	8	12	20	0	0
		lb/hr	tpy	header		0	0	0	0	0	0
	n-hexane	0.02060	0.09021	separator		2	12	24	20	0	
	benzene	0.00051	0.00224	meters/piping		0	0	0	0	0	0
	ethyl benzene	0.00004	0.00018	compressor		1	12	0	57	4	0
	toluene	0.00039	0.00172	dehydrator		0	0	0	0	0	0
	xylene	0.00020	0.00088		total		37	46	101	4	1

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ENGINE POTENTIAL EMISSIONS CALCULATIONS

		Heat Input			Emissions, tpy						GHG Emissions, tons/yr		
Engine No.	HP	mmBtu/hr	NOx	VOC	СО	SO2	TSP	PM10	PM2.5	CO2	CH4	N2O	CO2e
AA-002	165	1.22	11.83	0.16	19.91	0.00	0.05	0.10	0.10	624.23	1.18E-02	0.001	624.88
AA-002a	215	1.59	15.41	0.21	25.94	0.00	0.07	0.14	0.14	813.39	1.53E-02	0.002	814.23
	A STATE OF	Total	27.24	0.36	45.85	0.01	0.12	0.24	0.24	1437.62	0.03	0.00	1439.11

Pollutant	AP-42 Emission Factor	Conversion Factor, g to lbs
	lbs/MMBtu	0.0022046
NOx	2.21	CO2
/OC	0.0296	CH4
co	3.72	N2O
502	0.000588	
PM10	0.00950	
PM2.5	0.00950	
PM cond	0.00991	

ENGINE HAP EMISSIONS CALCULATIONS

	Natural Gas	AA-	002	AA-(002a
	Emission Factor,	HAP EMISSIONS		HAP EMISSIONS	
HAP	lbs/mmBtu	lbs/hr	tpy	lbs/hr	tpy
1,1,2,2-Tetrachloroethane	2.53E-05	3.09E-05	1.35E-04	4.03E-05	1.76E-04
1,1,2-Trichloroethane	1.53E-05	1.87E-05	8.19E-05	2.44E-05	1.07E-04
1,3-Butadiene	6.63E-04	8.10E-04	3.55E-03	1.06E-03	4.62E-03
1,3-Dichloropropene	1.27E-05	1.55E-05	6.80E-05	2.02E-05	8.86E-05
Acetaldehyde	2.79E-03	3.41E-03	1.49E-02	4.44E-03	1.95E-02
Acrolein	2.63E-03	3.21E-03	1.41E-02	4.19E-03	1.83E-02
Benzene	1.58E-03	1.93E-03	8.46E-03	2.52E-03	1.10E-02
Carbon Tetrachloride	1.77E-05	2.16E-05	9.47E-05	2.82E-05	1.23E-04
Chlorobenzene	1.29E-05	1.58E-05	6.90E-05	2.05E-05	9.00E-05
Chloroform	1.37E-05	1.67E-05	7.33E-05	2.18E-05	9.55E-05
Ethylbenzene	2.48E-05	3.03E-05	1.33E-04	3.95E-05	1.73E-04
Ethylene Dibromide	2.13E-05	2.60E-05	1.14E-04	3.39E-05	1.49E-04
Formaldehyde	2.05E-02	2.50E-02	1.10E-01	3.26E-02	1.43E-01
Methanol	3.06E-03	3.74E-03	1.64E-02	4.87E-03	2.13E-02
Methylene Chloride	4.12E-05	5.03E-05	2.20E-04	6.56E-05	2.87E-04
Naphthalene	9.71E-05	1.19E-04	5.20E-04	1.55E-04	6.77E-04
PAH	1.41E-04	1.72E-04	7.55E-04	2.24E-04	9.83E-04
Styrene	1.19E-05	1.45E-05	6.37E-05	1.89E-05	8.30E-05
Toluene	5.58E-04	6.82E-04	2.99E-03	8.88E-04	3.89E-03
Vinyl Chloride	7.18E-06	8.77E-06	3.84E-05	1.14E-05	5.01E-05
Xylene	1.95E-04	2.38E-04	1.04E-03	3.10E-04	1.36E-03
Total		3.96E-02	1.73E-01	5.16E-02	2.26E-01

AA-002 heat input=

1.22 mmBtu/hr

AA-002a heat input=

1.59 mmBtu/hr

annual operating hours=

8760

Emission factors from AP-42, Table 3.2-3

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Truck Loading Emissions Calculations 30-Day Average production

Basis: 30 day average production rates

L_L = 12.46 *(SPM)/T

(from EPA AP-42 Section 5.2.2.1)

Where:

L_L = Loading loss, lbs per 1,000 gal of liquid loaded

S = Saturation factor

P = True vapor pressure of liquid, psia M = Molecular weight of vapors, lb/lb-mole

T = Temperature of bulk liquid loaded, degrees R

CRUDE OIL

EPA "S"	True VP of	Mol. Wt. Of	Temp.	Sales Volume	Loading Rate	Uncontrolled Estimat Emissions,		
Factor	Liquid	Vapors	Liquid			Total	Hydrocar	bons
	(psia)	(lb/lb- mole)	°(R)	(10 ³ gal/yr)	(gal/hr)	Lı	(lb/hr)	(tpy)
1.45	5	48.00	545	3,311	16,000	7.96	127.30	13.17

PRODUCED WATER

-		1-4	ion
L.A	CH	ıaı	IOL

ı	EPA	True VP	Mol. Wt.	Temp.	Loaded	Loading	Uncont	rolled Es	timated
ı	"S"	of	Of	of	Volume	Rate	E	missions	3,
n	Factor	Liquid	Vapors	Liquid			Total	Hydrocar	rbons
		(psia)	(lb/lb- mole)	*(R)	(10 ³ gal/yr)	(gal/hr)	L	(lb/hr)	(tpy)
	1.45	0.05	48.00	545	153	16,000	0.08	1.27	0.01

HAPs	tons/yr
Benzene	0.057897
Toluene	0.057327
e-Benzene	0.00221
Xylenes	0.030194
n-hexane	0.392304
	0.539932

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Truck Loading Emissions Calculations, Maximum Ibs/hr

 $L_L = 12.46 * (SPM)/T$

(from EPA AP-42 Section 5.2.2.1)

Where:

L_L = Loading loss, lbs per 1,000 gal of liquid loaded

S = Saturation factor

P = True vapor pressure of liquid, psia
M = Molecular weight of vapors, lb/lb-mole
T = Temperature of bulk liquid loaded, degrees R

CRUDE OIL

EPA "S" Factor	True VP of Liquid	Mol. Wt. Of Vapors	of	Sales Volume	Loading Rate	Uncontrolled Estin Emissions, Total Hydrocarbo		3,
	(psia)	(lb/lb- mole)	*(R)	(10 ³ gal/hr)	(gal/hr)	Lı	(lb/hr)	
1.45	5	48.00	545	16.0	16,000	7.96	127.30	

PRODUCED WATER

Calculation

			Commence of the Commence of th		Loaded	The County of th	The second second second		
	"S"	of	Of	of	Volume	Rate		missions	Marie Control
on	Factor	Liquid	Vapors	DESCRIPTION OF THE PARTY NAMED IN			Total	Hydrocar	bons
		(psia)	(lb/lb- mole)	°(R)	(10 ³ gal/hr)	(gal/hr)	j	(lb/hr)	
	1.45	0.05	48.00	545	16.0	16,000	0.08	1.27	

HAPs	lbs/hr
Benzene	0.564848
Toluene	0.559285
e-Benzene	0.021562
Xylenes	0.294576
n-hexane	3.82734
total	5.267611

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External Combustion Equipment Emissions Calculations

	Capacity		Emissions, tons/yr					GHO	Emissions	metric tor	is/yr		
Source	MMBtu/hr	PM	PM10	Pm 2.5	NOx	СО	VOC	SO2	HAP	CO2	CH4	N20	CO2e
Heater Trea	0.5	0.004	0.016	0.016	0.215	0.180	0.012	0.001	0.004	255.45	0.00	0.00	255.72
Line Heate	0.25	0.002	0.008	0.008	0.107	0.090	0.006	0.001	0.000	127.73	0.00	0.00	127.86
Totals		0.006	0.024	0.024	0.322	0.271	0.018	0.002	0.004	383.18	0.01	0.00	383.58

Ap-42 natural gas	combustion
Emission Factors	Ibs/MMRtu

Limbore	on ractors, rospitalistic
Pm	0.001863
PM10	0.007451
PM2.5	0.007451
NOx	0.098039
CO	0.082353
VOC	0.005392
SO2	0.000588
HAPs	0.001851

40 CFR 98, subpart C

CH4 0.001	
N2O 0.0001	

Natural Gas Combustion HAP Calculations

	Natural Gas	Heater Treater		Flare Pilot		Line Heater		
	Emission Factor,	HAP EN	HAP EMISSIONS		HAP EMISSIONS		HAP EMISSIONS	
HAP	lbs/mmBtu	lbs/hr	tpy	lbs/hr	tpy	lbs/hr	tpy	
Benzene	2.06E-06	1.03E-06	4.51E-06	1.03E-07	4.51E-07	5.15E-07	2.25E-06	
Dichlorobenzene	1.18E-06	5.88E-07	2.58E-06	5.88E-08	2.58E-07	2.94E-07	1.29E-06	
Formaldehyde	7.35E-05	3.68E-05	1.61E-04	3.68E-06	1.61E-05	1.84E-05	8.05E-05	
Hexane	1.76E-03	8.82E-04	3.86E-03	8.82E-05	3.86E-04	4.41E-04	1.93E-03	
Naphthalene	5.98E-07	2.99E-07	1.31E-06	2.99E-08	1.31E-07	1.50E-07	6.55E-07	
Polycyclic Organic Matter	2.38E-05	1.19E-05	5.21E-05	1.19E-06	5.21E-06	5.95E-06	2.61E-05	
Toluene	3.33E-06	1.67E-06	7.30E-06	1.67E-07	7.30E-07	8.33E-07	3.65E-06	
Total		9.35E-04	4.09E-03	9.35E-05	4.09E-04	4.67E-04	2.05E-03	

Burner Heat Input=

0.50 mmBtu/hr

Flare Pilot Heat Input=

0.05 mmBtu/hr

Line Heater Heat Input= annual operating hours=

0.25 8760

Emission factors from AP-42, Table 1.4-3

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FLARE PILOT CALCULATIONS

Emission	Combustion	Capacity		Criteria Emissions, tons/yr						
Unit ID	Source	ммвтин	PM	PM10	PM2.5	NOx	CO	VOC	SO2	HAP
AA-001a	Flare (Pilot)	0.05	0.000	0.002	0.002	0.021	0.018	0.001	0.000	0.000

Emission	Combustion	Capacity	GHG	GHG Emissions, metric tons/yr				Emission	s, short ton	s/yr
Unit ID	Source	ммвтин	CO2	CH4	N2O	CO2e	CO2	CH4	N2O	CO2e
AA-001a	Flare (Pilot)	0.05	23.223	0.000	0.000	23.246	25.59	0.00	0.00	25.62

Gas combustion

AP-42 Em	ission Factors, lbs/MMBtu	Emission Factors, kg/MMBt		
TSP	0.001863	CO2	53.02	
PM10	0.007451	CH4	0.001	
PM2.5	0.007451	N2O	0.0001	
NOx	0.098039			
CO	0.082353			
VOC	0.005392			
SO2	0.000588			
HAPs	0.001851			

MDEQ NOTICE OF INTENT FOR COVERAGE UNDER THE OIL PRODUCTION GENERAL PERMIT TO CONSTRUCT/OPERATE AIR EMISSIONS EQUIPMENT AT A SYNTHETIC MINOR SOURCE					
Compliance Plan Section OPGP-G					
Part 1. Equipment List					
List all equipment and the corresponding federal and/or state regulation that is applicable. Clearly identify federal regulations from state requirements. Provide the expected or actual construction date, startup date and removal date if the equipment is no longer on site.					

EMISSION UNIT (Ref No.)	FEDERAL or STATE REGULATION Ex. 40 CFR Part, Subpart Ex. 11 Miss. Admin. Code Pt. 2, R. 1.4.B(2).	CONSTRUCTION DATE	STARTUP DATE	REMOVAL DATE
AA-000 Well affected facility	40 CFR 60, Subpart OOOOa			
AA-002a	40 CFR 60 Subpart JJJJ	3/01/25	3/01/25	

Compliance Plan

Section OPGP-G

Part 2. Applicable Requirements

List all applicable state and federal requirements, including emission limits, operating restrictions, etc., and the applicable test methods or monitoring used to demonstrate compliance with each applicable requirement. Clearly identify federal regulations from state requirements. Provide the compliance status as of the day the application is signed.

EMISSION UNIT (Ref No.)	APPLICABLE REQUIREMENT (Specific Regulatory citation)	POLLUTANT	LIMITS/ REQUIREMENTS	TEST METHOD/ COMPLIANCE MONITORING
Example: Compressor	Item 8 of Table 2d of 40 CFR 63, Subpart ZZZZ	HAPs	Change oil and filter every 2,160 hours of operation or annually, whichever comes first; Inspect spark plugs every 2,160 hours of operation or annually, whichever comes first, and replace as necessary; and Inspect all hoses and belts every 2,160 hours of operation or annually, whichever comes first, and replace as necessary.	Monitoring of compressor hours of operation
Example: Tanks	40 CFR 60.5395(a)(2)	VOC and Methane	Must reduce VOC emissions by 95.0 percent within 60 days after startup of production.	Tank emissions are routed to the flare for destruction at all times of operations.
Example: Flare	11 Miss. Admin. Code Pt. 2, R.1.4.B(2).	H₂S	1 grain H ₂ S per 100 standard cubic feet (1 gr/100 scf)	Recordkeeping of H2S composition of gas by gas analysis; Maintenance of continuous flame for gas combustion.
This list of exampl	es is not intended to be conclusive for each type of	emission source. Thi	is list only provides examples of how the ta	ble should be completed.
AA-001, Flare & facility wide	1 Miss. Admin. Code Pt. 2, R.1.4.B(2).	H₂S	Any gas stream containing as much as 1 grain H ₂ S per 100 standard cubic feet (1 gr/100 scf) must be incinerated prior to discharge to the atmosphere	Recordkeeping of H2S composition of gas by gas analysis; Maintenance of continuous flame for gas combustion.
AA-002, AA-002a, Engines,	40 CFR 63, subpart ZZZZ, (§63.6590(a))	НАР	Applicability	Applicability Only
AA-002,	40 CFR 63, subpart ZZZZ, (§63.6603 & Table 2(d))	НАР	Change oil and filter every 1,440 hours of operation or annually, whichever comes first; b. Inspect spark plugs every	Monitoring engine hours of operation

Compliance Plan Section OPGP-G

Part 2. Applicable Requirements

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EMISSION UNIT (Ref No.)	APPLICABLE REQUIREMENT (Specific Regulatory citation)	POLLUTANT	LIMITS/ REQUIREMENTS	TEST METHOD/ COMPLIANCE MONITORING
			1,440 hours of operation or annually, whichever comes first, and replace as necessary c. Inspect all hoses and belts every 1,440 hours of operation or annually, whichever comes first, and replace as necessary.	
AA-002,	40 CFR 63, subpart ZZZZ, (§63.6605)	НАР	Contiuous compliance and General Duty to operate and maintain in a manner consistent with safety and good air pollution control practies to minimize emissions	Process Knowledge
AA-002,	40 CFR 63, subpart ZZZZ, (§63.6640 (a) and Table 6)	НАР	i. Operating and maintaining the stationary RICE according to the manufacturer's emission-related operation and maintenance instructions; or ii. Develop and follow your own maintenance plan	Process Knowledge
AA-002	40 CFR 63, subpart ZZZZ, (§63.6655 (a),(d) and (e))	НАР	Recordkeeping Requiremnts	Recordkeeping
AA-002	40 CFR 63, subpart ZZZZ, (§63.6660 (a),(b) and (c))	НАР	General recordkeeping requirements	Recordkeeping
AA-002,	40 CFR 63, subpart ZZZZ, (§63.6640 (b)	НАР	Report any failure to perform a required work practice as scheduled	Reporting
AA-002	40 CFR 63, subpart ZZZZ, (§63.6665 (a) and Table 8)	НАР	Applicable requirements under 40 CFR 63 subpart A	Applicability

Compliance Plan Section OPGP-G

Part 2. Applicable Requirements

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EMISSION UNIT (Ref No.)	APPLICABLE REQUIREMENT (Specific Regulatory citation)	POLLUTANT	LIMITS/ REQUIREMENTS	TEST METHOD/ COMPLIANCE MONITORING
AA-003 Fugitive Emissions	40 CFR 60.5365a(i)	VOC and Methane	Applicability	Applicability only
AA-003 Fugitive Emissions	40 CFR 60.5397a(a-g)	VOC and Methane	Develop a fugitive emission monitoring plan	Upon Startup
AA-003 Fugitive Emissions	40 CFR 60.5397a(h)	VOC and Methane	Fugitive emission source repair or replacement requirements	Written Plan development
AA-003 Fugitive Emissions	40 CFR 60.5425a and Table 3	VOC and Methane	Applicability of General Provisions of 40 CFR 60, Subpart A	Applicability only
AA-003 Fugitive Emissions	40 CFR 60.5410a(j)	VOC and Methane	Demonstration of initial compliance	Monitoring
AA-003 Fugitive Emissions	40 CFR 60.415a(h)	VOC and Methane	Demonstration of continuous compliance	Monitoring
AA-003 Fugitive Emissions	40 CFR 60.5420a(c)	VOC and Methane	Recordkeeping requirements	Monitoring and Recordkeeping
AA-003 Fugitive Emissions	40 CFR 60.5420a(b)	VOC and Methane	Reporting requirements	Reporting
AA-008 Storage Tanks	40 CFR 60.5365a(e)	VOC and Methane	Applicability determination may take into account legally and practically enforceable limit on tank emissions	Applicability Only. Federally enforceable limit requested for avoidance.

Compliance Plan Section OPGP-G

Part 2. Applicable Requirements

List all applicable state and federal requirements, including emission limits, operating restrictions, etc., and the applicable test methods or monitoring used to demonstrate compliance with each applicable requirement. Clearly identify federal regulations from state requirements. Provide the compliance status as of the day the application is signed.

EMISSION UNIT (Ref No.)	APPLICABLE REQUIREMENT (Specific Regulatory citation)	POLLUTANT	LIMITS/ REQUIREMENTS	TEST METHOD/ COMPLIANCE MONITORING
AA-000 Well affected facility	40 CFR 60.5365a(a)	voc	Applicability	Process Knowledge
AA-000 Well affected facility	40 CFR 60.5375a(a)	VOC	Completion standards/procedures for VOC control	Process Knowledge
AA-000 Well affected facility	40 CFR 60.5410a(a) 40 CFR 60.5415a(a)	voc	Submit notification, annual report, maintain log of records, as applicable	Recordkeeping and Reporting
AA-000 Well affected facility	40 CFR 60.5420a	voc	Specific notification, recordkeeping and reporting requirements.	Recordkeeping and Reporting
AA-002a	40 CFR 60.4230(a)(4)(iii) and 60.4246(a), Subpart JJJJ	NOx, CO, VOC	Applicability	
AA-002a	40 CFR 60.4233(e), 60.4234, and Table 1, Subpart JJJJ	NOx, CO, VOC	NOx ≤ 2.0 g/hp-hr (160 ppmvd @ 15 % O2) • CO ≤ 4.0 g/hp-hr (540 ppmvd @ 15 % O2) • VOC ≤ 1.0 g/hp-hr (86 ppmvd @ 15 % O2) 1	Initial stack test, follow manufacturer's operation and maintenance plan
АА-002а	40 CFR 60.4243(b)(2)(i) and 60.4244, Subpart JJJJ; 40 CFR 60.8(a), Subpart A; and 11 Miss. Admin. Code Pt. 2, R. 2.2.B(11).	NOx, CO, VOC	Initial performance testing and routine maintenance	Initial stack test, follow manufacturer's operation and maintenance plan
AA-002a	40 CFR 60.4245(a)(1), (2), and (4), Subpart JJJJ	NOx, CO, VOC	Records	Maintain records of notifications, maintenance, and performance testing